AMENDMENTS TO THE DRAWINGS

Appended hereto as attachments are replacement formal drawing sheets to replace the drawings that were included in the PCT application. The PCT drawings have only been amended to replace the handwritten figure designations and reference numerals with typographical characters.

1829

REMARKS

The substitute specification together with the amended claims and

amended drawings place the present U.S. national phase application in better form

for examination on the merits.

Based upon the specification, drawing, and claim amendments to this

national phase application, it is believed that the amended specification, the amended

drawings, and the amended claims conform with U.S. formal requirements. Early and

favorable action on this application is respectfully requested.

Should the examiner have any question after considering this Preliminary

Amendment, he is cordially invited to telephone the undersigned attorney so that any

such question can be quickly resolved in order that the present application can

proceed toward allowance.

Respectfully submitted,

January 5, 2006

Alfred J Mangels

Reg. No. 22,605

4729 Cornell Road

Cincinnati, Ohio 45241

Tel.: (513) 469-0470

Attachments: Attachment A

Attachment B

Replacement drawing sheets including changes



ATTACHMENT B

SUBSTITUTE SPECIFICATION

(Showing All Changes Made to the Specification and Abstract in International Application No. PCT/SE2005/001194)

A METHOD PERTAINING TO COMBUSTION, AND A BURNER

BACKGROUND OF THE INVENTION

والخب

FIELD OF THE INVENTION

The present invention relates to a method pertaining to combustion, and to a burner. More specifically, the invention relates to a method and to a burner for the combustion of oxygen gas in respect of heating furnaces.

DESCRIPTION OF THE RELATED ART

When combusting hydrocarbons in combination with high oxygen concentration concentrations, flame temperatures in excess of 2000 degrees C are normally reached, together with furnace atmospheres of very high partial pressures of carbon dioxide and steam. This results in drawbacks, such as high NOx NOx -contents and local overheating problems.

It is highly desirous to design burners that have emission_diminishing properties. The present invention satisfies this desideratum that desire.

SUMMARY OF THE INVENTION

Accordingly, the present invention relates to a method pertaining to the combustion of a fuel with an oxidant in a heating furnace, where wherein the fuel and the oxidant are delivered to a burner head , and is characterized in that in . In a first method step fuel and oxydant oxidant are caused to be emitted from the burner head

in the close proximity of one another, so that the process of combustion will take process takes place essentially close to and at a small distance out away from the burner head until there a temperature is reached in the furnace space a temperature that exceeds the spontaneous combustion temperature of the fuel and in that in . In a second method step the fuel and the oxidant are then caused instead to be emitted from the burner head in mutually spaced relationship, so that the process of combustion will take process takes place essentially at a distance from the burner head corresponding to at least the diameter of the burner head and out away from the burner head.

The invention also relates to a burner of the kind and with the general features set forth in claim 9 head that includes a fuel supply nozzle and a first oxidant outlet opening in close proximity to the fuel nozzle, so that combustion takes place close to and at a small distance away from the burner head. The burner head also includes further oxidant outlet openings that are located at a distance from the fuel nozzle, so that combustion takes place at a distance from the burner head corresponding to at least the diameter of the burner head and outward of the burner. The burner is adapted to deliver the oxidant at an overpressure of at least 2 bar.

BRIEF DESCRIPTION OF THE DRAWINGS

The invention will now be described in more detail, partly with reference to exemplifying embodiments of the invention illustrated in the accompanying drawings, in which:

- Fig. 1 is a straight-on, front view of a burner head according to a first embodiment;
- Fig. 2 is a straight-on , front view of a burner head according to a second embodiment;
- Fig. 3 is a diagrammatic illustration of a burner head and a flame as seen from one side when the burner is operated in a first manner; and
- Fig. 4 is a diagrammatic illustration of a burner head and a flame as seen from one side when the burner is operated in a second manner.

DESCRIPTION OF THE PREFERRED EMBODIMENTS

The inventive method thus pertains relates to the combustion of a fuel with an oxidant in a heating furnace, in which the fuel and the oxidant are delivered to a burner head. The burner head is mounted in a known matter manner in a furnace wall, so that the flame produced in the combustion process will extend into the furnace chamber.

The invention is characterized in that the combustion process takes place in two steps, where the second step affords advantages over the known technology.

In a first method step, fuel and oxidant are emitted from the burner head in close relationship with one another, so that the process of combustion will essentially take takes place close to and slightly spaced from the burner head. This method is known per se, in which the burner is designated as an "Oxy-fuel" -burner.

In this first step of the method, the burner is operated until a temperature exceeding the spontaneous combustion temperature of the fuel is reached in the furnace chamber.

The second step of the combustion process may can conveniently be initiated when the furnace temperature is above roughly 750 degrees C.

According to the invention, this second method step is carried out when this that temperature or a still higher temperature has been reached. In this second method step, the fuel and the oxidant are caused instead to be emitted from the burner head at a distance from each other, so that combustion will take takes place generally at a distance from the burner head that corresponds at least to the diameter of the burner head and out away from the burner head.

It is preferred that in the first method step the fuel is caused to be emitted from a <u>fuel</u> nozzle 2 in the burner head 1, and the oxidant is caused to be emitted from <u>oxidant</u> outlet openings 3 placed concentrically around the <u>fuel</u> nozzle 2; see <u>figure</u>, as shown in Figure 1.

It is also preferred that in the second method step, the fuel is caused to be emitted from a <u>fuel</u> nozzle 2 in a <u>the</u> burner head 1, and that the oxidant is emitted from <u>oxidant</u> outlet openings 4, 5 located on one side of and at a distance from <u>said</u> <u>fuel</u> nozzle 2 ; see figure, as shown in Figure 1.

According to one preferred embodiment of the invention, the <u>oxidant</u> outlet openings 4, 5 are comprised of Laval nozzles or venturi-nozzles.

The opening 6 functions to monitor the flame.

According to one preferred embodiment of the invention, the <u>oxidant</u> outlet openings 4, 5 are spaced from the fuel nozzle 2 by <u>at</u> a distance that exceeds half the diameter of the burner head.

It has been found that a distance of about 40 mm suffices to afford provide the desired effect.

The burner thus permits two different *modus operandi*, partly as a typical oxyfuel burner and partly as a burner which functions to produce a flame of essentially lower maximum temperature. This That lower flame temperature is adapted to lie beneath be less than the temperature at which the formation of NOx NO_x is limited by the reaction kinetics, this that temperature being about 1550 degrees C.

This That result is achieved by the aforesaid above-mentioned placement of the exygen oxidant outlet openings 4, 5 and the fuel nozzle 2, whereby fuel and oxygen are combusted further away from the burner head in comparison with a conventional oxy-fuel-combustion process. This That result is illustrated in figures Figures 3 and 4, where figure wherein Figure 3 illustrates the mutual relationship between the length and the propagation of the flames flame 7 -8 in the respect of oxy-fuel-combustion, and figure Figure 4 illustrates the mutual relationship between the length and the propagation of said flames flame 8 in the case of combustion according to the second step of the inventive method.

The concept of the invention resides in lowering the oxygen content in the combustion zone, despite the oxidant having an oxygen content of more than 80%, by virtue of separation, high pressure, and an optimized nozzle placement. This That is achieved with a nozzle burner head configuration that affords results in a high subpressure on those surfaces of the nozzle burner head 1 that lack medium-emitting nozzles. As a result of the that subpressure, flue gases are sucked in from the furnace atmosphere and quickly mix with the out-flowing outflowing media and therewith create

turbulence. The mixing medium, i.e., the furnace atmosphere, typically has an oxygen content of 0.5 - 10%. The remainder of the gas is comprised of CO_2 and H_2O and N_2 in varying mixtures proportions.

Because CO_2 , H_2O_1 and N_2 do not actively take part in the combustion process, these those constituents act as "combustion retardants." [[.]] The dilution of the oxygen and the fuel is very high. Typically, oxygen concentrations of 7 - 15 % are reached in the combustion process, despite the use of pure oxygen. When applying the present invention there is obtained at process temperatures above said the spontaneous combustion temperature a diffused but controlled combustion that significantly lowers the formation NO_2 of NO_2 gases, primarily NO_2 and NO_2 .

As a result, fuel and oxidant will be are mixed with the furnace flue gases before the fuel and oxidant gases meet one another. This gives That provides a larger and colder flame 8 in spite of the efficacy corresponding to that achieved when combustion is effected according to known technology. The nozzles fuel nozzle 2 and oxidant openings 3, 4, and 5 can be directed conveniently directed straight forward, i.e., they need not be directed away from or towards each other, although they may can be angled towards or away from the longitudinal axis of the burner head.

According to one preferred embodiment of the inventive method, the oxydant oxidant is gaseous and is given at an oxygen concentration of 85% or higher.

According to one significant feature of the inventive method, the oxidant is delivered to the burner at a pressure of at least 2 bar overpressure. Because the flame temperature is lower and the mixture of gas in the furnace volume is greater than in the case of oxy-fuel-combustion, the formation of $\frac{NO_x}{NO_x}$ is minimized while

the temperature differences in the furnace space are dramatically lowered at the same time.

In comparison with conventional combustion devices used in industrial processes, application of the inventive method results in a lowering of $\frac{NO_x}{NO_x}$ formations by more than 90 %, without impairing the efficiency of the process and without the supply of substances other than those required for the combustion.

A burner nozzle head according to the present invention is no larges larger than a known burner head for oxy-fuel-combustion. In a preferred embodiment of the invention, the burner nozzle head has a diameter of about 70 mm.

The compact method structure enables the invention to be applied in equipment already possessed by the user. Moreover, the equipment can be placed in a small, water-cooled protective casing for application at very high process temperatures.

The aforesaid above-mentioned advantages are achieved in accordance with the invention with a selected fuel, which can be solid fuel, gaseous fuel, or liquid fuel. The inventive arrangement can replace existing combustion systems in principal principle without re-constructing the furnace equipment used for the process.

It is beneficial when the fuel used is oil, propane, or natural gas.

The burner head shown in figure Figure 1 is intended for oil as the fuel.

Figure 2 shows a burner head 10 for natural gas as fuel. The <u>fuel</u> nozzle 11 is intended for natural gas. The outlet openings 12, 13, 14 are intended for the oxidant. The opening 15 is intended for monitoring the flame and the opening 16 is intended for a pilot flame.

Because the oxidant openings and the fuel nozzles can be directed straight forwards, there is obtained a construction burner head is achieved that is inexpensive, that is easy to maintain, and that can be applied in existing processes without requiring measures other than the exchange of the nozzle construction burner head.

The oxidant is injected into the combustion space via one or more nozzles oxidant openings in the form of Laval nozzles or venturi nozzles. The oxidant will preferably be under at an overpressure of at least 2 bar. The higher the pressure, the better the efficacy of the invention. A preferred pressure for normal applications is 4 - 5 bar. The fuel is injected via conventional <u>fuel</u> nozzles at the pressure available.

Although the invention has been described above with reference to a number of exemplifying embodiments it will be understood that the design of the burner head can be varied. For instance, the burner head may can include more oxidant outlet openings than those shown. Moreover, the placement of the fuel nozzle may can be different to from that shown in the drawings.

It will therefore be understood that the present invention is not restricted to the embodiments described above, but can be varied within the scope of the accompanying claims.

CLAIMS

What is claimed is:

ABSTRACT OF THE DISCLOSURE

The present invention relates to a A method pertaining and apparatus relating to the combustion of a fuel with an oxidant in a heating furnace, wherein the fuel and the oxidant are delivered to a burner head.

The invention is characterized in that in In a first method step fuel and oxidant are caused to be emitted from the burner head (1; 10) in the close proximity of to each other, so that combustion will essentially take takes place close to and at a small distance outward of the burner head, and until there a temperature is reached in the furnace space a temperature that exceeds the spontaneous combustion temperature of the fuel; and in that in In a second method step the fuel and the oxidant are caused to be instead emitted instead from the burner head (1; 10) at a mutual distance apart, so that combustion will essentially take takes place at a distance from the burner head corresponding to at least the diameter of the burner head and outwards outward of the burner head.

(Fig. 1 for publication)